Kinetic Theory of a Non-spherical Granular Intruder

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Non-spherical Granular Systems







Stationary granular gas



Intruder-bath particle collisions are inelastic with COR α < 1

Martin and Piasecki, 1999; Garzo and Dufty, 1999; Barrat and Trizac, 2002

Particle flux depends on surface velocity

$$P_{+}(U) = \frac{\Phi_{+}}{\Phi} = \frac{1}{2} \left(1 + \frac{U}{\Phi(U)} \right)$$

Kinetic Equation

Intruder particle velocity distribution

$$\Psi_+(V \to U) = \rho \int_{-\infty}^{V} dv (V - v) f(v, a) \delta(V - U + \frac{1 + \alpha}{1 + M}(v - V))$$

$$-\Phi(U)F(U) + \rho\left(\frac{1+M}{1+\alpha}\right)^2 \int_{-\infty}^{\infty} dV |U-V| f(V + \frac{1+M}{1+\alpha}(U-V), a)F(V) = 0$$

Solution

$$F(U) = \exp\left(-\frac{mU^2}{2\gamma T_B}\right)$$

The intruder particle possesses a stationary Maxwellian velocity distribution with an effective granular temperature $T_{eff} = \gamma T_B$

$$\gamma = \frac{1 + \alpha}{2 + (1 - \alpha) \frac{m}{M}} \le 1$$

Martin and Piasecki

Event driven simulation



Mean event rate

ED simulation





Needle System



Collision



Kinetic Theory

$$\frac{\partial f^{(1)}(v_1,\omega)}{\partial t} = \int dv_2 \int dr_2 \overline{T_{12}} f^{(2)}(v_1,\omega,v_2)$$

$$f^{(2)}(v_1, \omega, v_2) = f^{(1)}(v_1, \omega) \Phi(v_2)$$

$$\Phi(v_2) \propto \exp\left(-\frac{mv_2^2}{2T}\right)$$

Analysis

$$\frac{dT_T}{dt} \propto \int dr_2 \int dv_2 \int d\omega \int d\theta \overline{T_{12}} f^{(2)}(v_1, \omega, v_2) E_1^T = 0$$

$$\frac{dT_R}{dt} \propto \int dr_2 \int dv_2 \int d\omega \int d\theta \overline{T_{12}} f^{(2)}(v_1, \omega, v_2) E_1^R = 0$$

Maxwell distribution of needle angular and translational velocities is not a stationary state of the Enskog-Boltzmann Equation

But we use it as a trial function...

$$f^{(1)}(v_1, \omega_1) \propto \exp\left(-\frac{Mv_1^2}{2\gamma_T T} - \frac{I\omega_1^2}{2\gamma_R T}\right)$$

Collision Operator

$$T_{12} = \Theta(L/2 - |\lambda|)\delta(|\mathbf{r}_{12}.\mathbf{u}_{1}^{\perp}| - 0^{+}) \left| \frac{d |\mathbf{r}_{12}.\mathbf{u}_{1}^{\perp}|}{dt} \right| \Theta\left(-\left|\frac{d |\mathbf{r}_{12}.\mathbf{u}_{1}^{\perp}|}{dt}\right|\right)(b_{12} - 1)$$

contact flux approach difference

$$\lambda \mathbf{u}_{1}$$

Solution

Let
$$k = \frac{L^2}{4I(1/m + 1/M)}$$

$$b\int_{0}^{1} dx \frac{\sqrt{1+akx^{2}}}{1+kx^{2}} = \frac{1+\alpha}{2} \int_{0}^{1} dx \frac{(1+akx^{2})^{3/2}}{(1+kx^{2})^{2}} \qquad (1)$$

$$a\int_{0}^{1} dxx^{2} \frac{\sqrt{1+akx^{2}}}{1+kx^{2}} = \frac{1+\alpha}{2} \int_{0}^{1} dx \frac{x^{2}(1+akx^{2})^{3/2}}{(1+kx^{2})^{2}} \qquad (2)$$

$$a = \gamma_{R} \frac{M+m}{M+m\gamma_{T}} \qquad (3) \qquad b = \gamma_{T} \frac{M+m}{M+m\gamma_{T}} \qquad (4)$$

Solve (2) for *a*. Then find *b* from (1). Then find γ_R and γ_T from (3) and (4)

ED Simulation



Granular temperatures



Inhomogeneous Needle



Velocity distributions



Discorectangle



Steady State Solution

$$b[(1+\alpha_1)cI_1^{01}(a,k) + (1+\alpha_2)(1-c)J_1^{01}(a,k)] = \frac{(1+\alpha_1)^2}{2}cI_2^{03}(a,k) + \frac{(1+\alpha_2)^2}{2}(1-c)J_2^{03}(a,k)]$$

$$a[(1+\alpha_1)cI_1^{11}(a,k) + (1+\alpha_2)(1-c)J_1^{11}(a,k)] = \frac{(1+\alpha_1)^2}{2}cI_2^{13}(a,k) + \frac{(1+\alpha_2)^2}{2}(1-c)J_2^{13}(a,k)]$$

$$k = \frac{L^2}{4I\left(\frac{1}{m} + \frac{1}{M}\right)} \qquad c = \frac{L}{L + 2(r+R)}$$









Summary

- Theory gives results in excellent agreement with ED simulations
- Equipartition is generally not obtained except:
 - in the limit of light bath particles
 - If COR depends on position of impact
- For uniform COR, $T_R < T_T$
- Small deviations from gaussian
- Non equipartition also expected for higher dimensions and more complex shapes
- Experimental verification in 2D?