

Fluctuation Rheology Using a Polymer.

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Outline

1. Rheology measurement by looking at the fluctuations
2. Using polymer, why and how?
3. Summary

Fluctuation-dissipation theorem

A particle doing 1D Brownian motion, where $\hat{\eta}(t)$ is the thermal random force.

$$x(t) = \int_{-\infty}^t dt' \alpha(t-t') \hat{\eta}(t') \quad \text{or} \quad x(\omega) = \alpha(\omega) \hat{\eta}(\omega)$$

Callen, Welton, Kubo (1950s):

$$\langle \hat{\eta}(\omega) \hat{\eta}(-\omega) \rangle = \frac{2k_B T}{\omega} \text{Im} \left(\alpha^{-1}(\omega) \right) \underbrace{\left[\frac{\hbar\omega}{2k_B T} \coth \frac{\hbar\omega}{2k_B T} \right]}_{\approx 1 \text{ for small } \omega}$$

or

$$\langle x(\omega) x(-\omega) \rangle = \frac{2k_B T}{\omega} \alpha''(\omega)$$

Fluctuation Rheology (Gittes et. al. 97)

- Measure $\langle x(0)x(t) \rangle$. FT to get $\langle x(\omega)x(-\omega) \rangle$.
- Use FDT to get $\alpha''(\omega) = (\omega/2k_B T) \langle x(\omega)x(-\omega) \rangle$
- The real part can be obtained by Kramers & Kronig's formula

$$\alpha'(\omega) = \frac{2}{\pi} P \int_0^{\infty} d\xi \frac{\xi \alpha''(\xi)}{\xi^2 - \omega^2}$$

- For a spherical particle

$$\alpha(\omega) = \frac{1}{6\pi a G^*(\omega)} \quad \text{provided}$$

$$\sigma(t) = \int_{-\infty}^t G(t-t') \nabla \mathbf{v}(t') dt' \quad \text{where} \quad G^*(\omega) \equiv i\omega \int_0^{\infty} d\tau e^{-i\omega\tau} G(\tau)$$

Problems

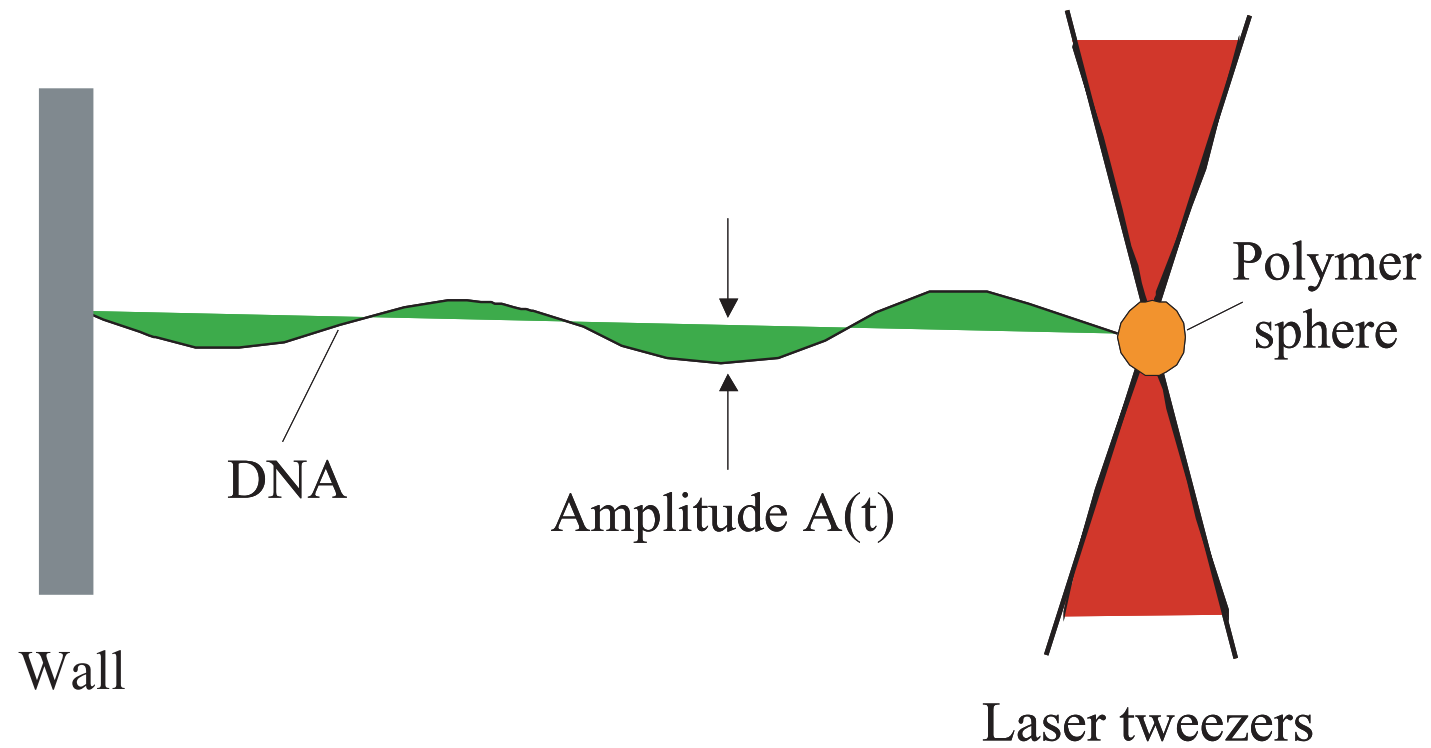
Rheological property depends on the length scale. Small sphere can only probe the Microrheology. How to do Macrorheology?

2 spheres, or

Using a Polymer to do Macrorheology

- Use the conformation degree of freedom to do fluctuation rheology.
- The test polymer can be very long. One can use the long wavelength mode to get the macrorheology.
- Can probe many wavelengths at the same experiment.

A possible experimental setup.



Length scale dependent viscoelasticity

Linear response regime.

- The stress $\sigma(\mathbf{r}, t)$ is proportional to the strain rate $\nabla\mathbf{v}(\mathbf{r}', t')$.

$$\sigma(\mathbf{r}, t) = \int \int_{-\infty}^t g(\mathbf{r} - \mathbf{r}', t - t') \nabla\mathbf{v}(\mathbf{r}', t') dt' d\mathbf{r}'$$

- The complex modulus can be defined as

$$G^*(\mathbf{k}, \omega) \equiv i\omega \int d\mathbf{r} \int_0^{\infty} d\tau e^{-i\omega\tau} e^{-i\mathbf{k}\cdot\mathbf{r}} g(\mathbf{r}, \tau)$$

- The macroscopic viscoelasticity is just $G^*(0, \omega)$ or written as $G^*(\omega)$.

Polymer Dynamic Equation

The Newton's 2nd law

$$\underbrace{\rho(\partial_t \mathbf{v} + \mathbf{v} \cdot \nabla \mathbf{v})}_{\text{inertia terms}} = -\nabla P - \frac{\delta F}{\delta \mathbf{r}} + \underbrace{\nabla \cdot \boldsymbol{\sigma}}_{\text{viscoelastic force}} + \underbrace{\hat{\eta}}_{\text{random noise}}$$

■ The polymer elastic force

$$-\frac{\delta F}{\delta \mathbf{r}} = \int ds \delta^3(\mathbf{r} - \mathbf{R}(s, t)) (\epsilon \mathbf{R}(s, t))$$

where $\epsilon \equiv (3k_B T/b) \partial_s^2$

■ Solve the flow field by FT on space and time.

$$\mathbf{v}(\mathbf{k}, \omega) \simeq \mathcal{G}(\mathbf{k}, \omega) \cdot \int \theta(\mathbf{k}, s) (\epsilon \mathbf{R}(s, \omega) + \hat{\eta}(s, \omega)) ds$$

$$\text{where } \mathcal{G}(\mathbf{k}, \omega) = \frac{i\omega(\mathbf{I} - \hat{\mathbf{k}}\hat{\mathbf{k}})}{\rho(i\omega)^2 + G^*(\mathbf{k}, \omega)k^2}, \quad \theta(\mathbf{k}, s) = e^{-i\mathbf{k} \cdot \mathbf{R}_0(s)}$$

Dispersion relation

polymer velocity

$$\overbrace{\partial_t \mathbf{R}(s, t)}^{\text{polymer velocity}} = \int d\mathbf{r} \delta^3(\mathbf{r} - \mathbf{R}(s, t)) \mathbf{v}(\mathbf{r}, t) \simeq \int \frac{d\mathbf{k}}{(2\pi)^3} \theta(\mathbf{k}, s) \mathbf{v}(-\mathbf{k}, t)$$

$$i\omega \mathbf{R}(s, \omega) \simeq \int \underbrace{\int \frac{d\mathbf{k}}{(2\pi)^3} \overbrace{\langle \theta(\mathbf{k}, s) \theta(-\mathbf{k}, s') \rangle}_{S(\mathbf{k}, s-s')}}_{\mathbf{H}(s-s', \omega)} \mathcal{G}(-\mathbf{k}, \omega) [\epsilon \mathbf{R}(s', \omega) + \hat{\eta}(s', \omega)] ds'$$

FT on $s \rightarrow q$ (the normal coordinate), the dispersion relation is

$$[i\omega + H_x(q, \omega)\epsilon(q)] R_x(q, \omega) = H_x(q, \omega)\hat{\eta}(q, \omega)$$

FDT:
$$\langle |R_x(q, \omega)|^2 \rangle = \frac{2k_B T}{\omega} \text{Im} \left[\frac{H_x(q, \omega)}{i\omega + H_x(q, \omega)\epsilon(q)} \right]$$

Structure function $S(\mathbf{k}, q)$

- The structure function $S(\mathbf{k}, q)$ is defined by

$$S(\mathbf{k}, q) = \int ds' \langle e^{-i\mathbf{k} \cdot (\mathbf{R}_0(s+s') - \mathbf{R}_0(s))} \rangle e^{-iqs'}$$

- For Gaussian chain under applied tension force F ,

$$S(\mathbf{k}, q) = \frac{12k^2/b}{k^4 + 4(k_z F/k_B T + 3q/b)^2}$$

- The applied tension can change $S(\mathbf{k}, q)$ (and possibly $\epsilon(q)$).

Mobility H_x

$$\begin{aligned}
 H_x(q, \omega) &= \underbrace{\frac{i\omega}{G^*(\omega)} \int \frac{d\mathbf{k}}{(2\pi)^3} \left(S(\mathbf{k}, q) \frac{(1 - \hat{k}_x^2)}{k^2} \right)}_{\text{Rouse}} \underbrace{\left(\frac{G^*(\omega)}{G^*(\mathbf{k}, \omega)} - 1 \right)}_{\substack{\text{universal at large } k \\ \text{vanishes at low } k}} \\
 &+ \underbrace{\frac{i\omega}{G^*(\omega)} \int \frac{d\mathbf{k}}{(2\pi)^3} S(\mathbf{k}, q) \frac{(1 - \hat{k}_x^2)}{k^2}}_{\text{Zimm} \propto q^{-1/2}} \\
 &+ \underbrace{\frac{i\rho\omega^3}{(G^*(\omega))^2} \int \frac{d\mathbf{k}}{(2\pi)^3} S(\mathbf{k}, q) \frac{(1 - \hat{k}_x^2)}{k^4}}_{\text{Inertia correction} \propto q^{-3/2}} \\
 &= \frac{i\omega}{G^*(\omega)} (h^R + h^Z(q)) + \delta H(q, \omega)
 \end{aligned}$$

Recipes

Drop the inertia effect first.

One can choose different q , or change the tension, so that $\epsilon(q)$ and $h(q)$ are different. Three measurements (at each ω) will give $G'(\omega)$, $G''(\omega)$, and h^R .

$$\langle |R_x(q, \omega)|^2 \rangle = \frac{2k_B T}{\omega} \frac{(h^R + h^Z(q))G''(\omega)}{[h^R\epsilon(q) + h^Z(q)\epsilon(q) + G'(\omega)]^2 + G''^2(\omega)}$$

Inertia correction can be included by the iteration process.

Summary

Advantages of fluctuation rheology using a polymer

- Can do macrorheology.
- Elastic coupling provides more data than the two spheres method. One can avoid the analytical continuation completely.
- The applied tension provides a new controlled parameter.
- In principle one can measure the anisotropic properties by changing the orientations of the probing polymer.

Disadvantages

- Have to calibrate $\epsilon(q)$ and $S(\mathbf{k}, q)$.
- Still can't measure the system with the slow modes.