

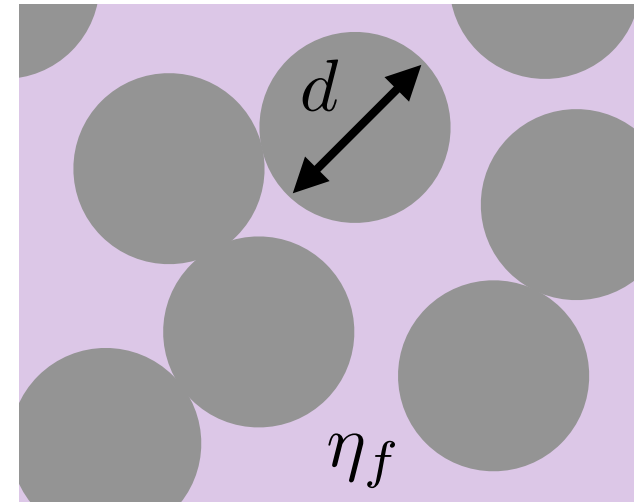


# Granular dispersion rheology as constraint counting

**B. M. Guy**, J. A. Richards, D. Hodgson, E. Blanco  
and W. C. K. Poon

# Granular dispersions: simple, right?

- Hard particles with  $d \gtrsim 2 \mu\text{m}$
- Non-Brownian (  $Pe \rightarrow \infty$  )
- Viscous flow (negligible particle and fluid inertia)



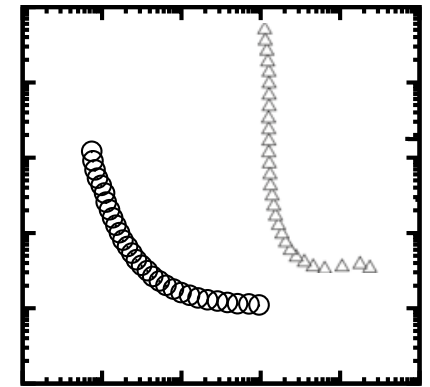
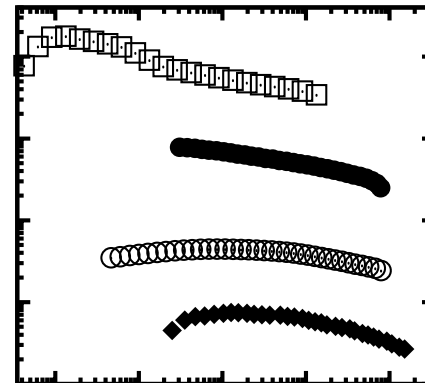
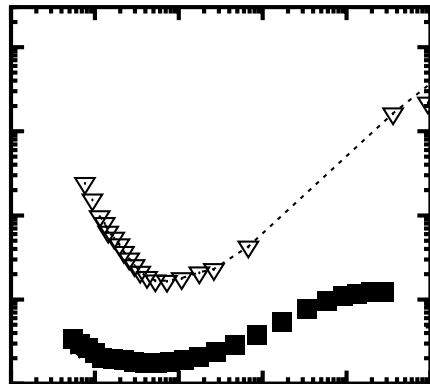
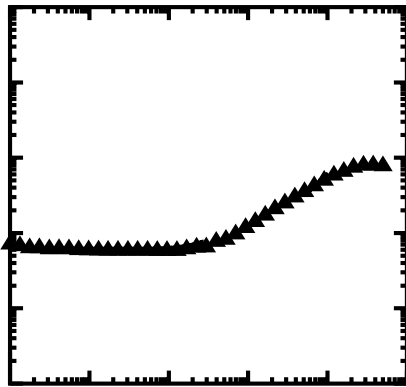
Expectation: universal, *Newtonian* rheology:

$$\text{Dimensional analysis} \implies \eta = \eta_f f(\phi) \propto \dot{\gamma}^0$$

# Reality:

Experimental phenomenology is *capricious*

Viscosity  $\eta$



Shear stress  $\sigma$

Guy et. al., PRL (2016)

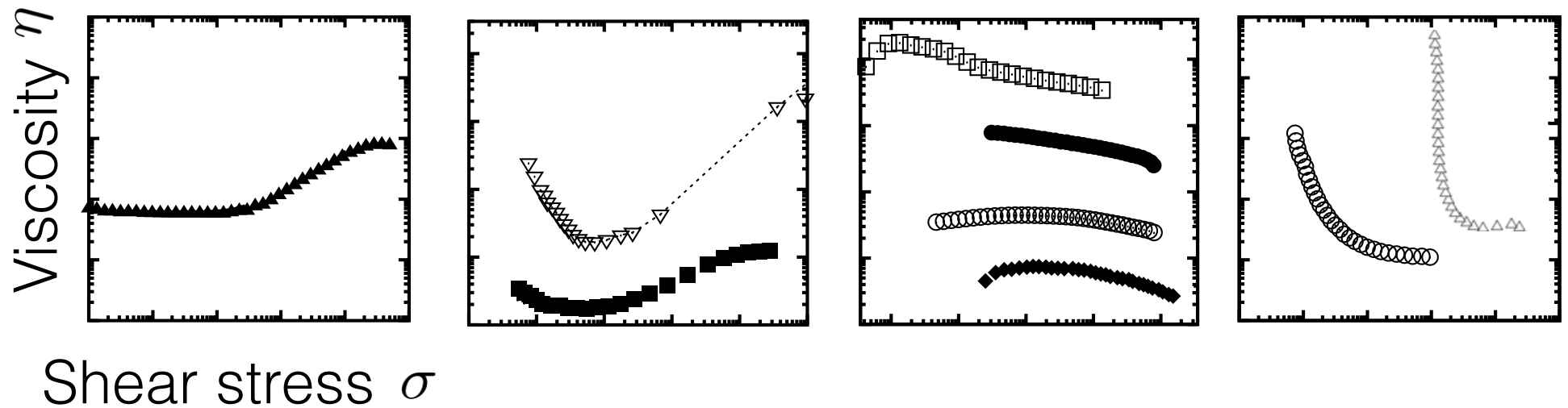
Zarraga et. al., J.  
Rheol. (2000)

Gamonpilas et. al., J.  
Rheol. (2016)

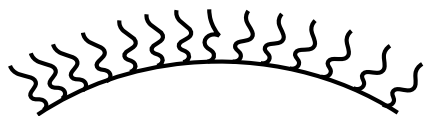
Brown & Jaeger, Nat.  
Mater. (2010)

Reality:

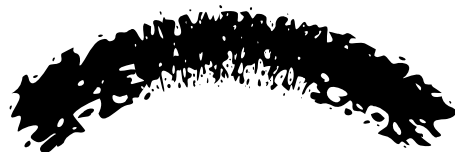
Experimental phenomenology is *capricious*



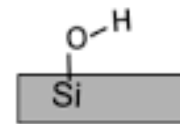
**Particle-level** details are important



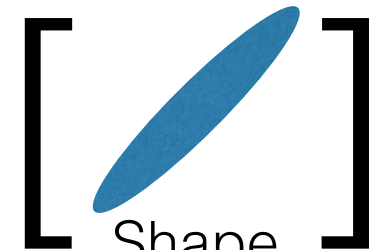
Polymer



Surface topology

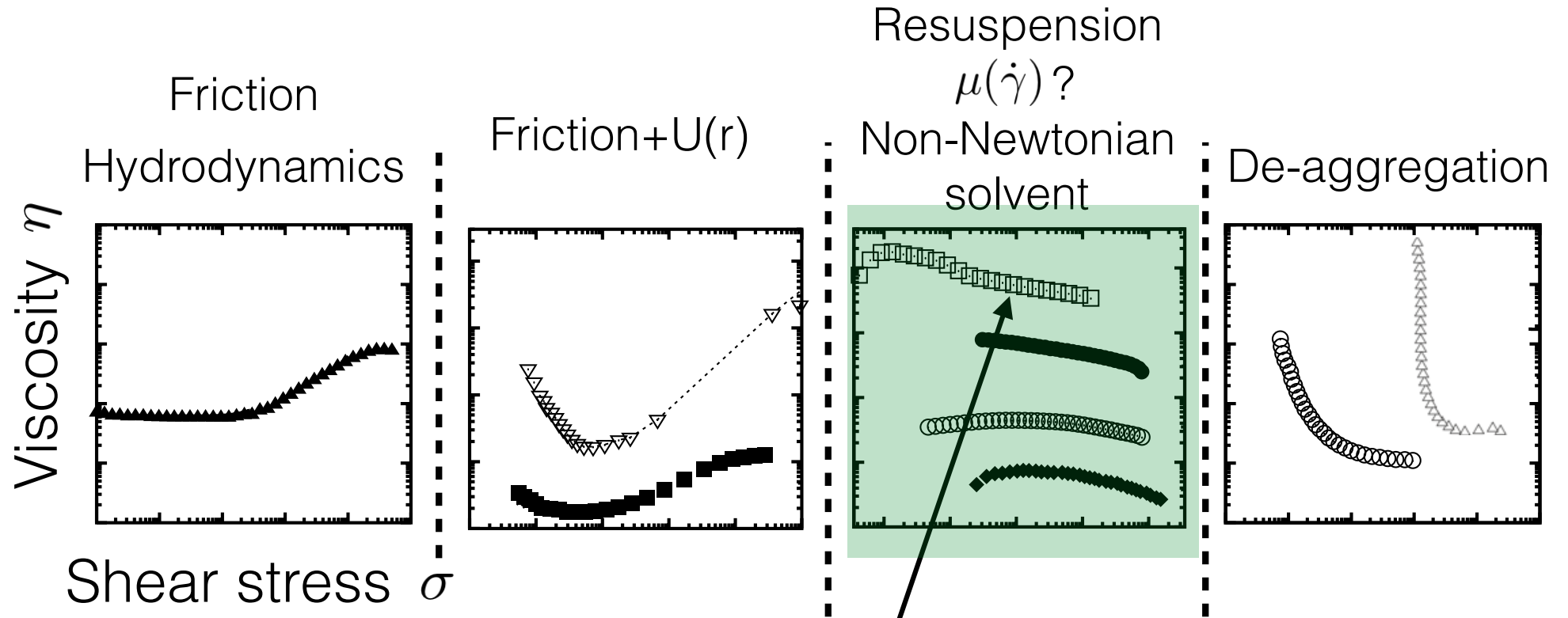


Surface chemistry



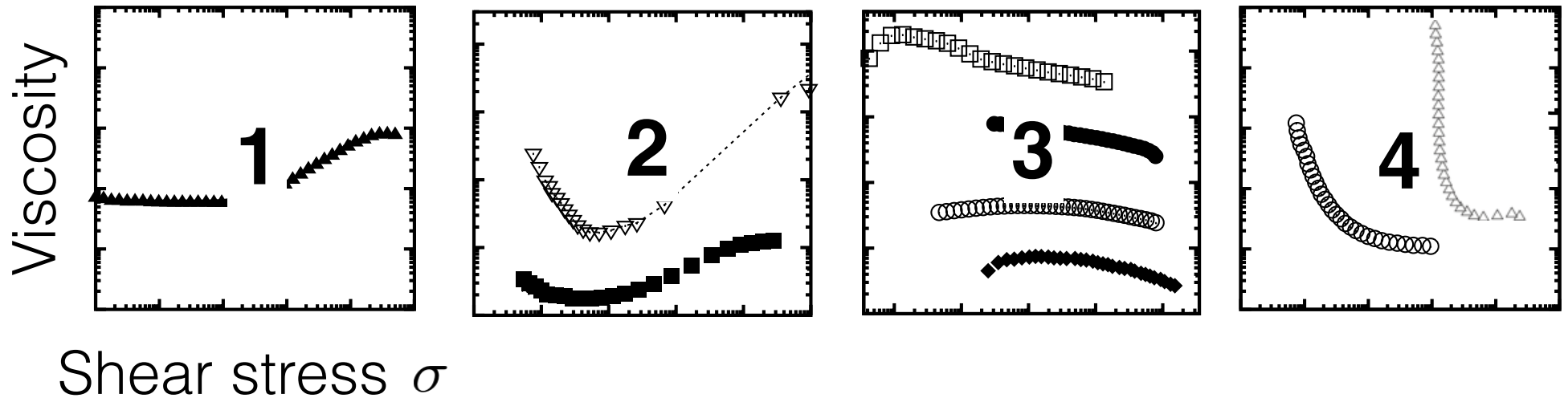
Shape

In most cases, explanations are bespoke



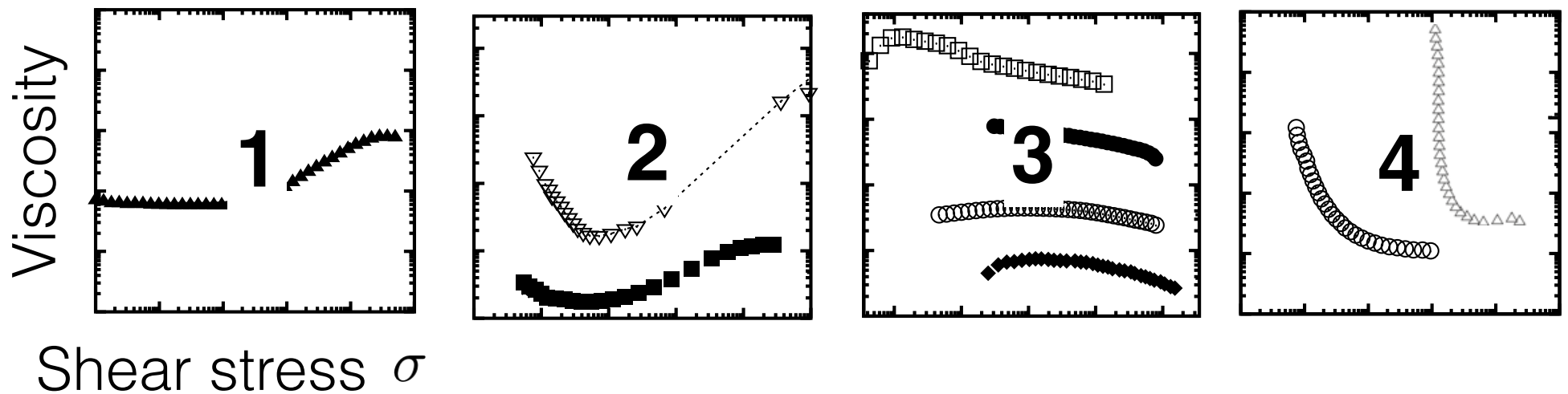
... and highly debated

# Is there a generic, underlying physics?



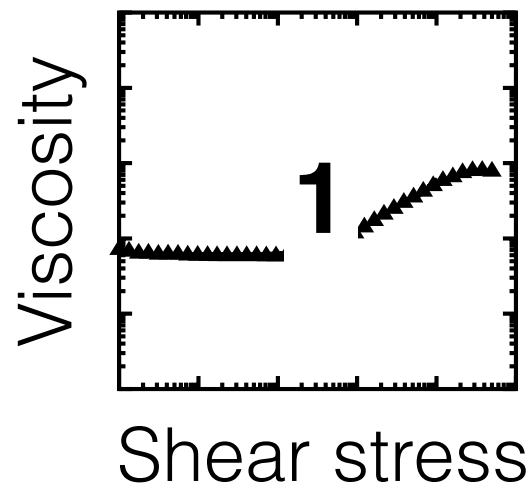
Connection?

Granular dispersion rheology is about making and breaking of **constraints** with stress



Details  $\rightarrow \mathcal{Z}(\sigma)$

# Wyart and Cates theory: constraint-driven version



Borrow ideas from dry  
granular packings



# Reformulated phenomenological WC theory (3-d)

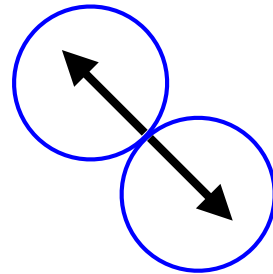
## Isostaticity:

Minimum number of contacts per sphere  $\mathcal{Z}$  for mechanical stability

# force/torque balance **equations** per particle = # force/torque **degrees of freedom** per particle

Frictionless

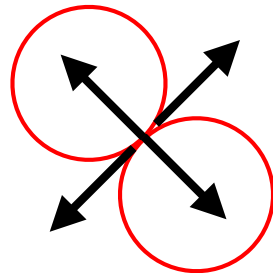
$$\mu = 0$$



$$\mathcal{Z} = 6$$

Frictional

$$\mu > 0$$



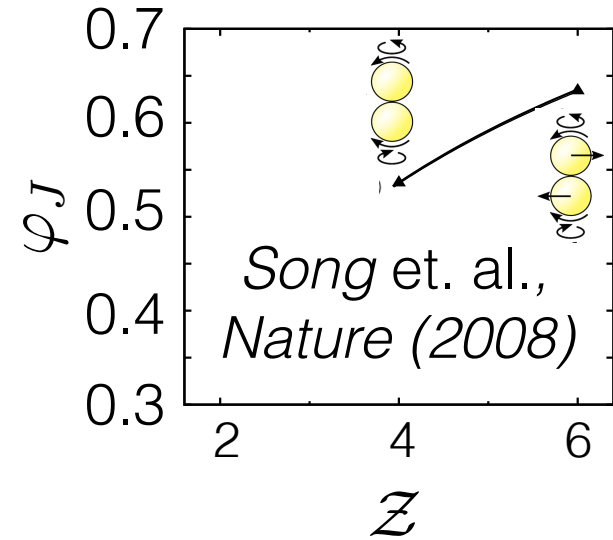
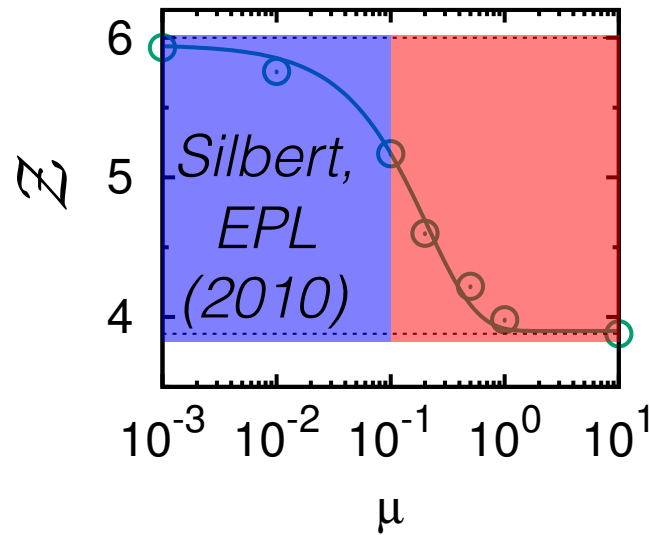
$$\mathcal{Z} = 4$$

Constrains sliding

# Reformulated phenomenological WC theory (3-d)

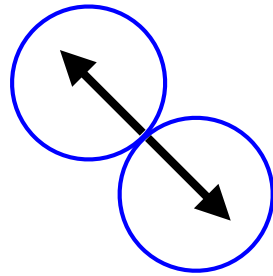
In practice:

Frictionless Frictional



Frictionless

$$\mu \ll 0.1$$



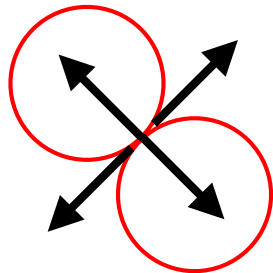
$$Z \approx 6$$

$$\rightarrow \phi_J^{(6)} \approx 0.64$$

(RCP)

Frictional

$$\mu \gg 0.1$$



$$Z \approx 4$$

$$\rightarrow \phi_J^{(4)} \approx 0.54$$

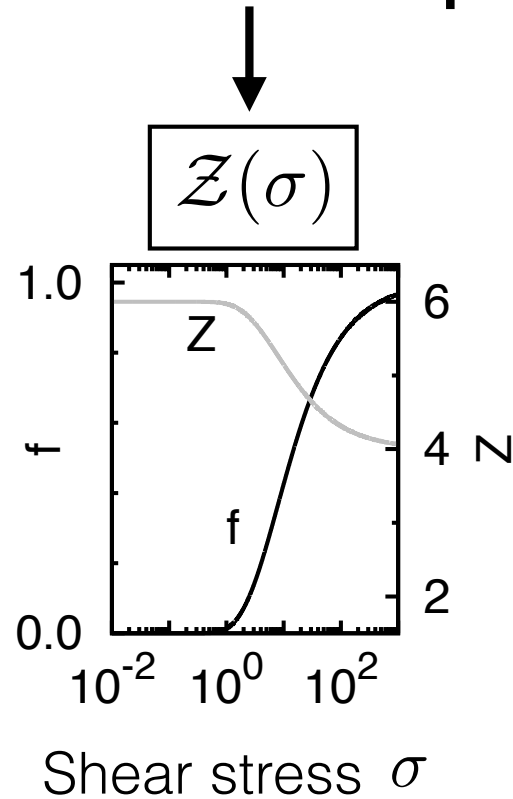
(RLP)

Dry packing



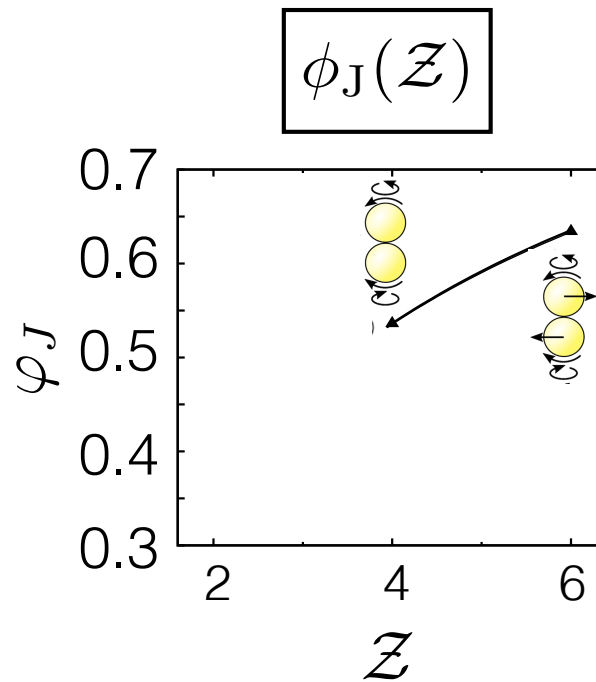
Sheared suspension

### Stress-dependent isostatic coordination number



$$Z = 6 - 2f$$

$$f(\sigma) = e^{-\left(\frac{\sigma^*}{\sigma}\right)^\beta}$$



$$\phi_J = \frac{Z}{Z + C}$$

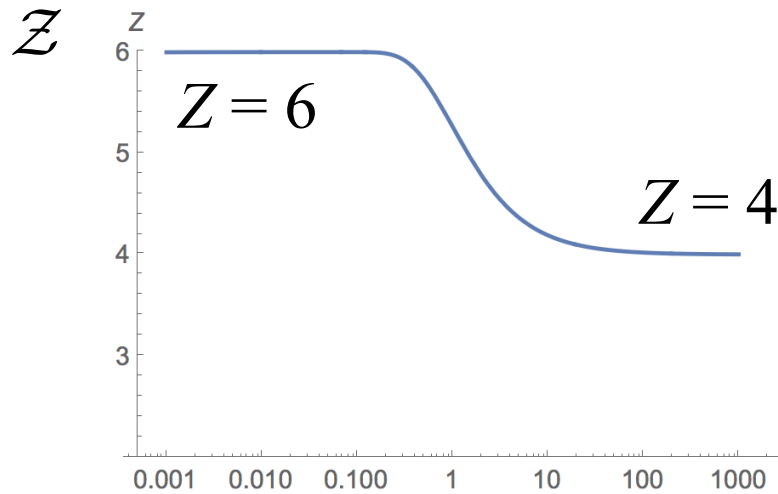
$$= 2\sqrt{3} \text{ for monodisperse spheres}$$

$\eta(\phi_J(Z))$

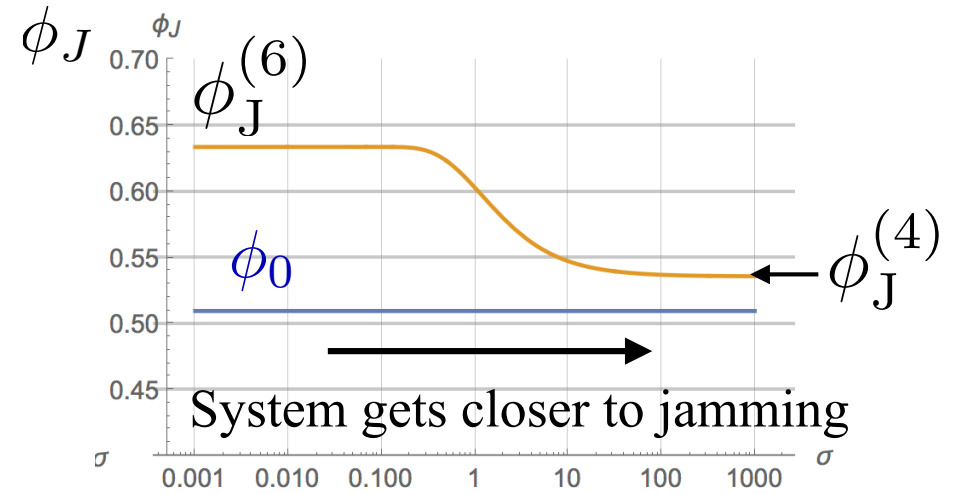
$$\eta = \left(1 - \frac{\phi}{\phi_J}\right)^{-2}$$

$$\eta(\sigma, \phi; \beta, \sigma^*, C)$$

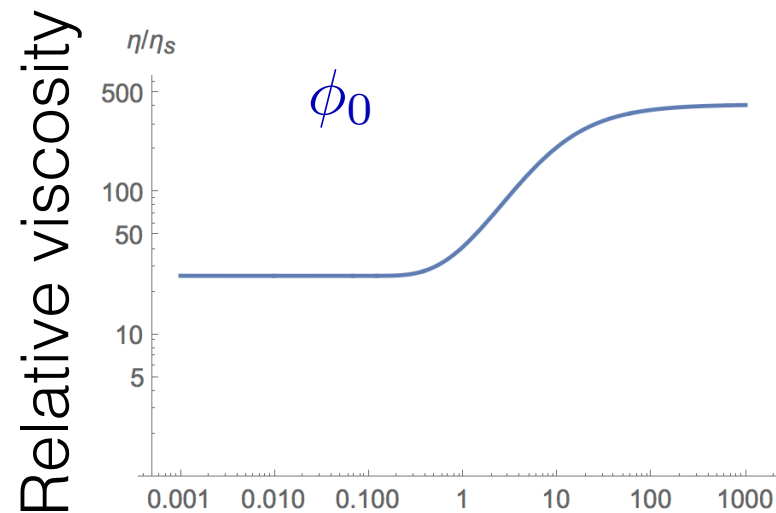
# Walkthrough: $\phi_0 < \varphi_J^{(4)}$



Shear stress

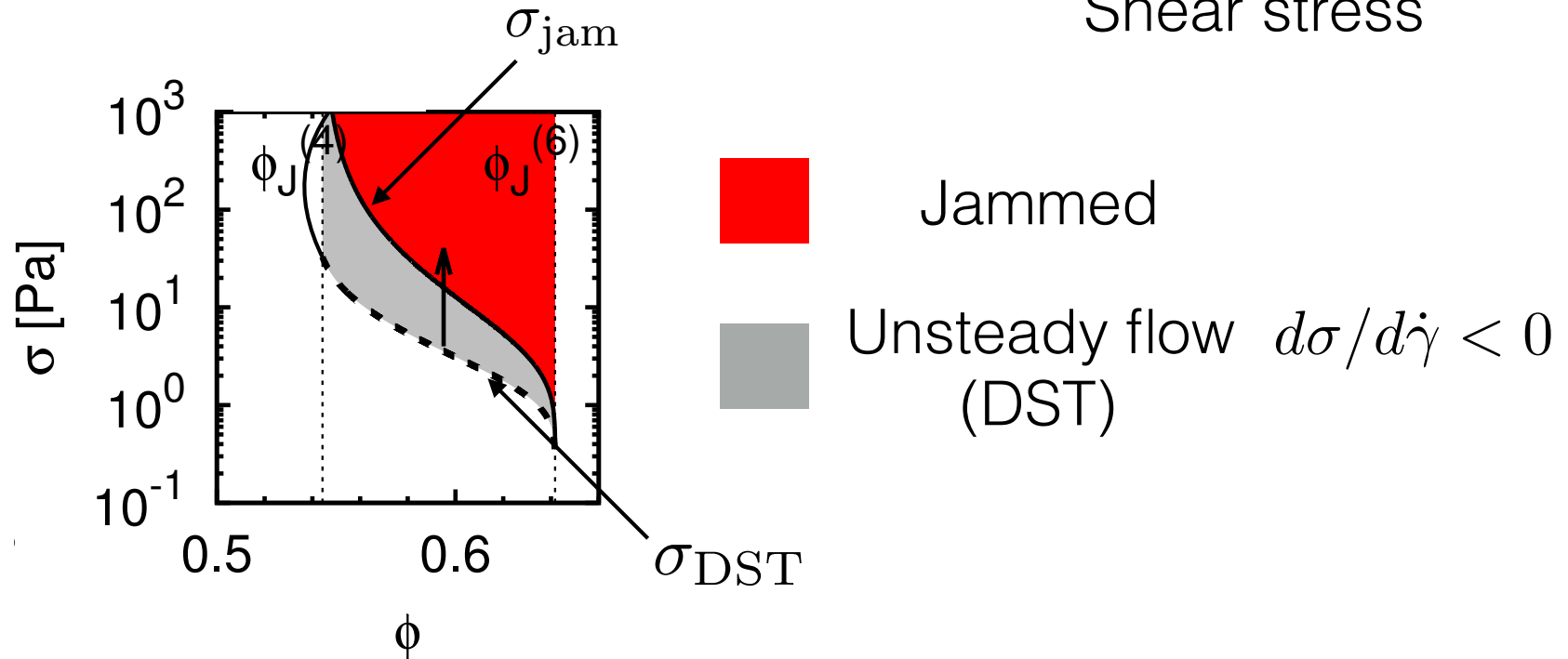
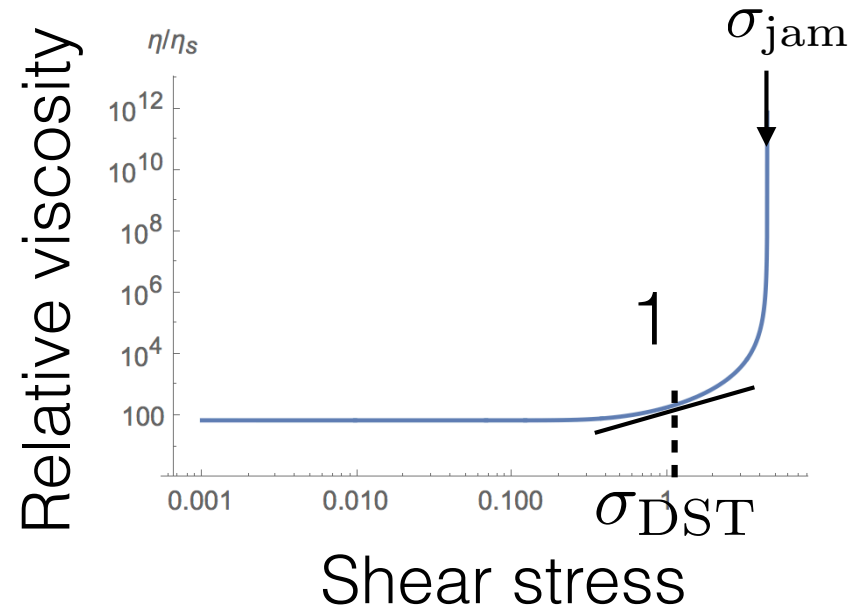
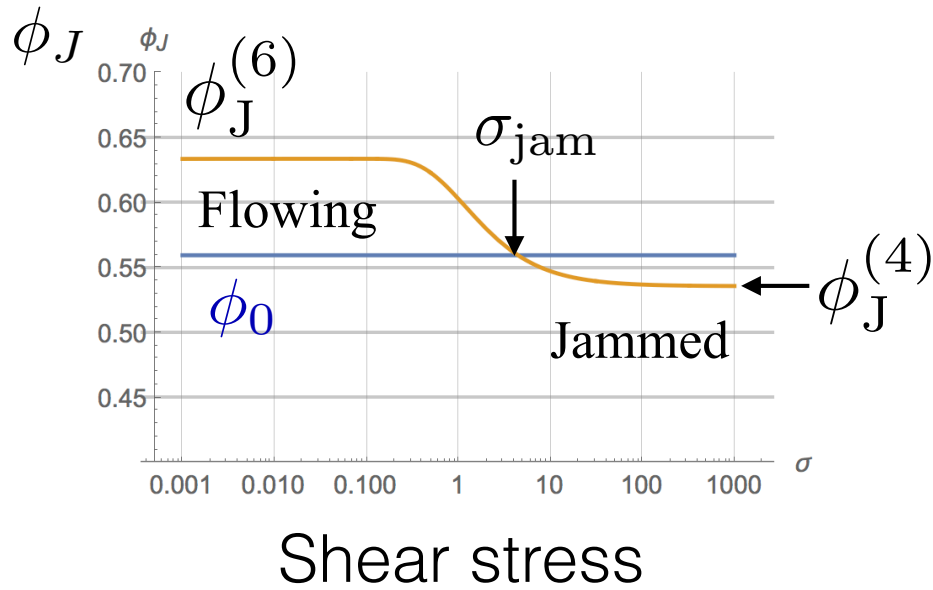


Shear stress

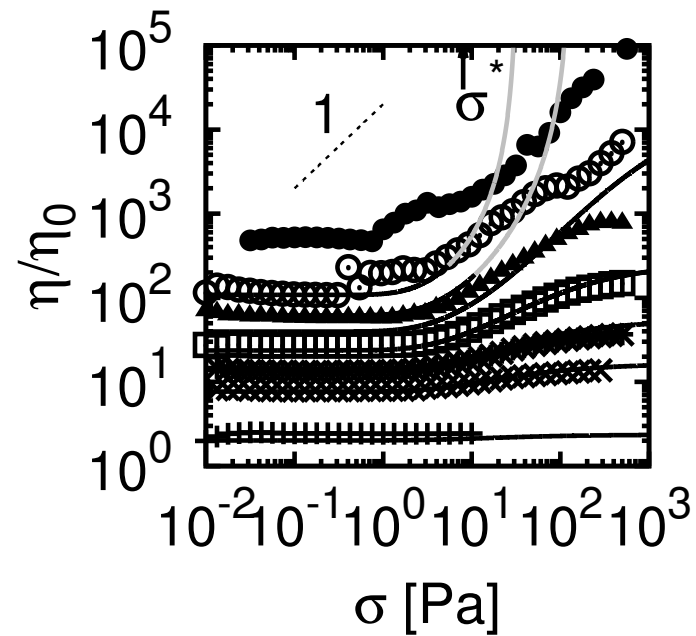


Shear stress

# Walkthrough: $\phi_0 \geq \phi_J^{(4)}$



## Example: 4 micron PMMA in CXB+decalin



*Guy, Hermes and Poon, PRL (2015)*

- ✓ Quantitatively captures experimental phenomenology

# Real particles are usually sticky!

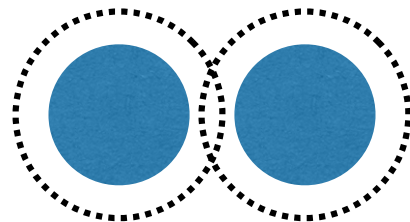
(e.g., due to van der Waals interactions)

**BUT**

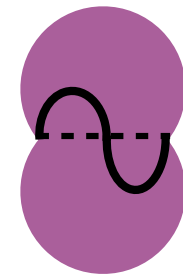
Attraction resulting from a central potential

$U_{\text{vdW}}(r)$  *does not* constrain rotations

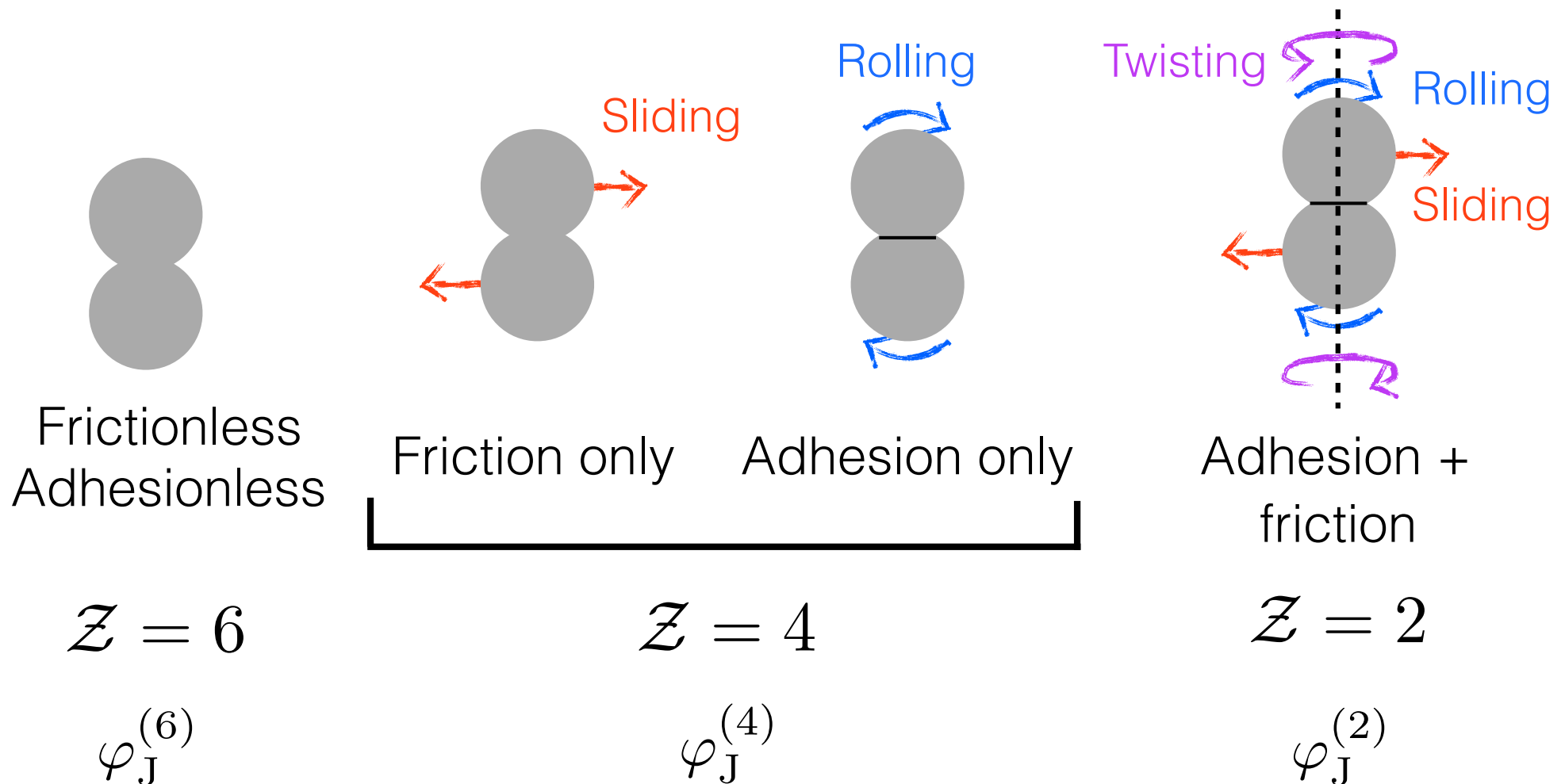
$\implies \mathcal{Z}$  unaffected



# Adhesion: rotations cost energy



Literature unclear for friction + adhesion. We propose:





# WC-like theory

Fraction of adhesive contacts  $a(\sigma) = 1 - e^{-(\sigma_A/\sigma)^\kappa}$

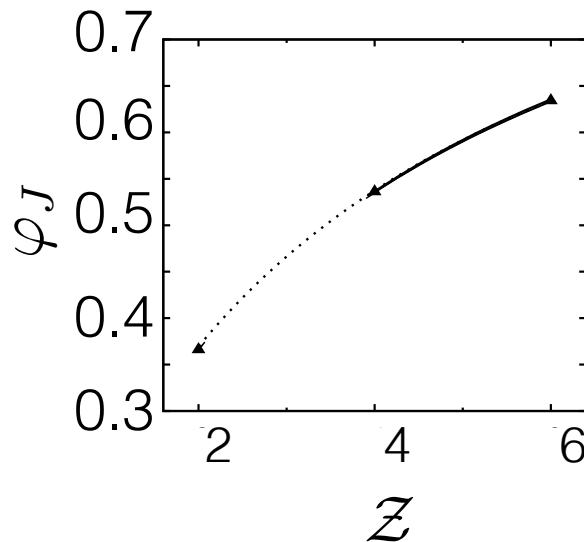
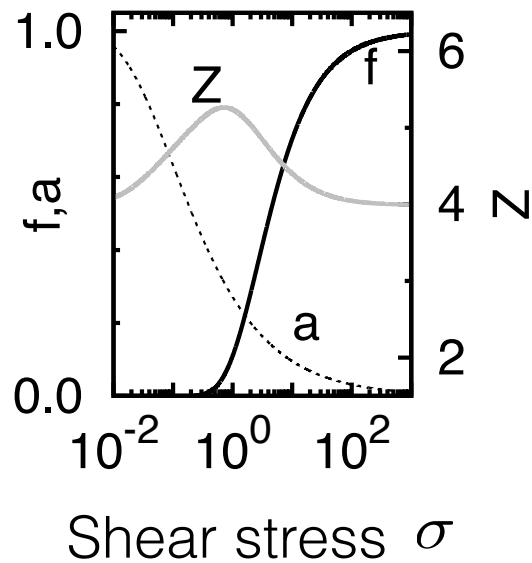
$\sigma_A$  = Characteristic adhesive stress

Fraction of frictional contacts  $f(\sigma) = e^{-(\sigma^*/\sigma)^\beta}$

$$\mathcal{Z} = 6 - 2f - 2a$$

$$\phi_J = \frac{\mathcal{Z}}{\mathcal{Z} + C}$$

$$\eta = \left(1 - \frac{\phi}{\phi_J}\right)^{-2}$$



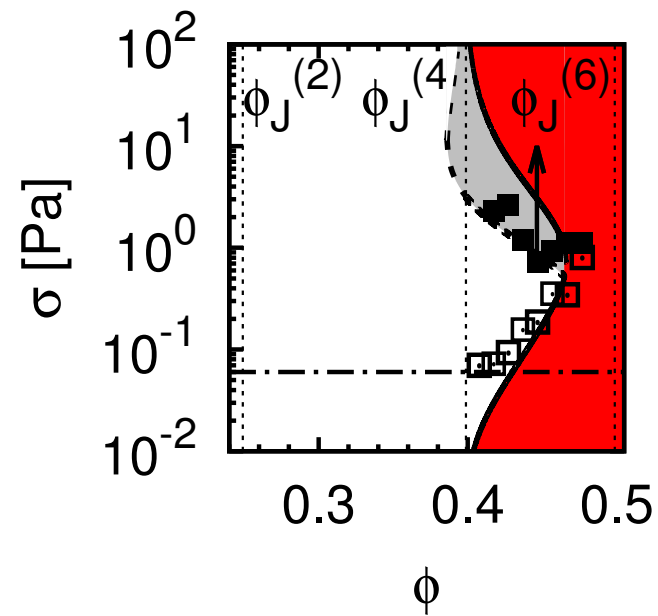
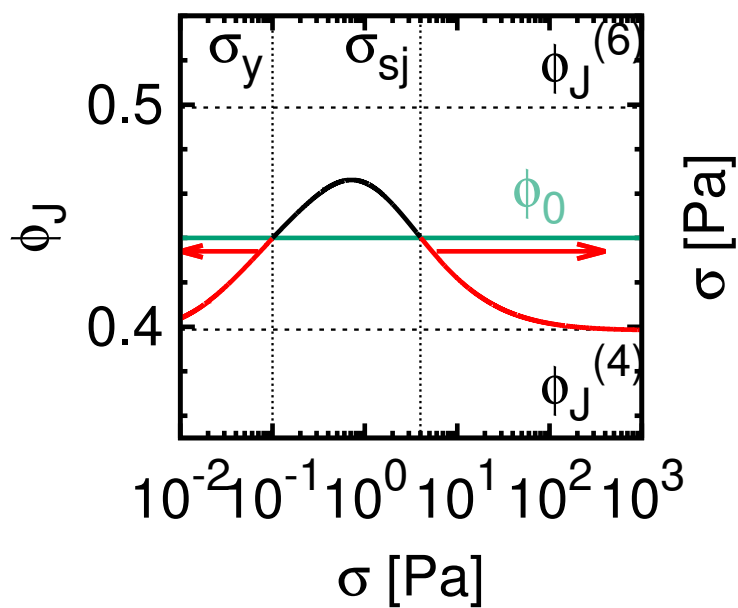
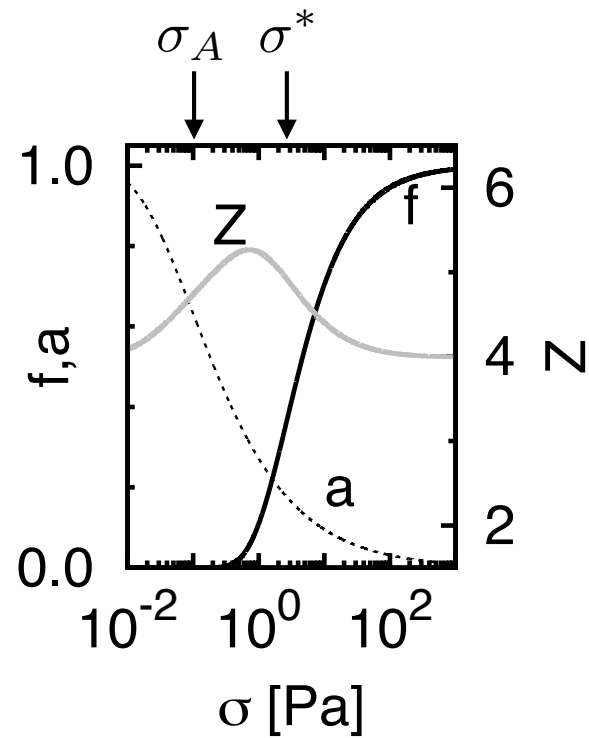
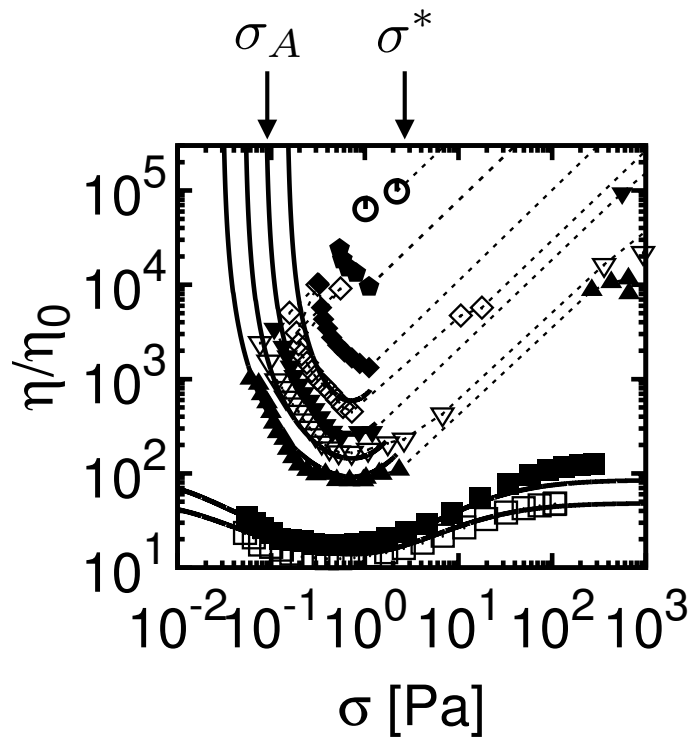
Details depend on

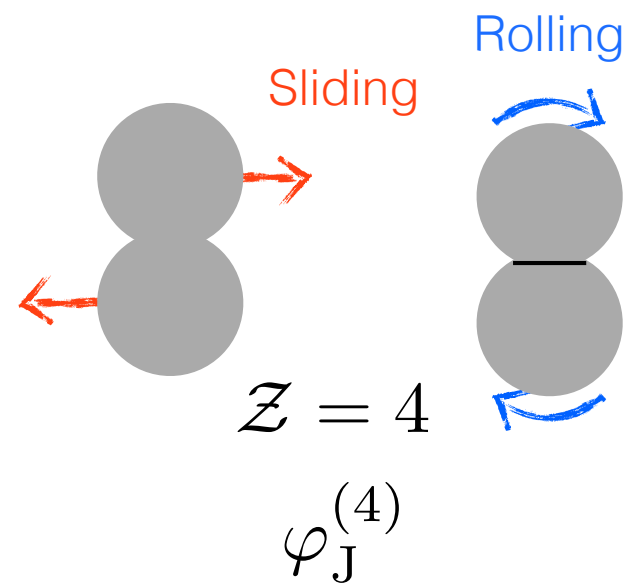
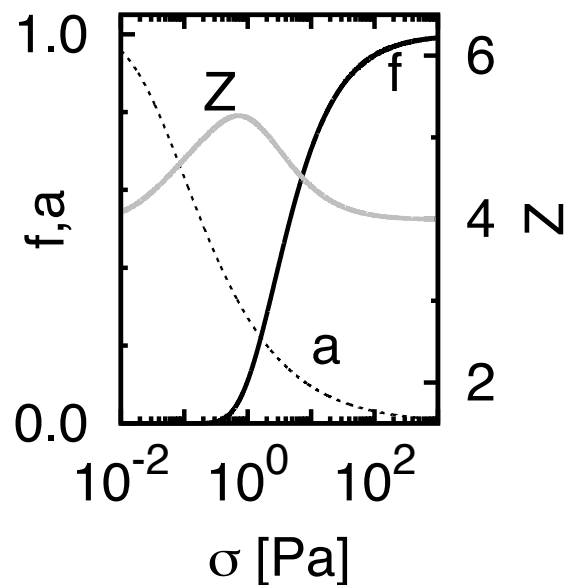
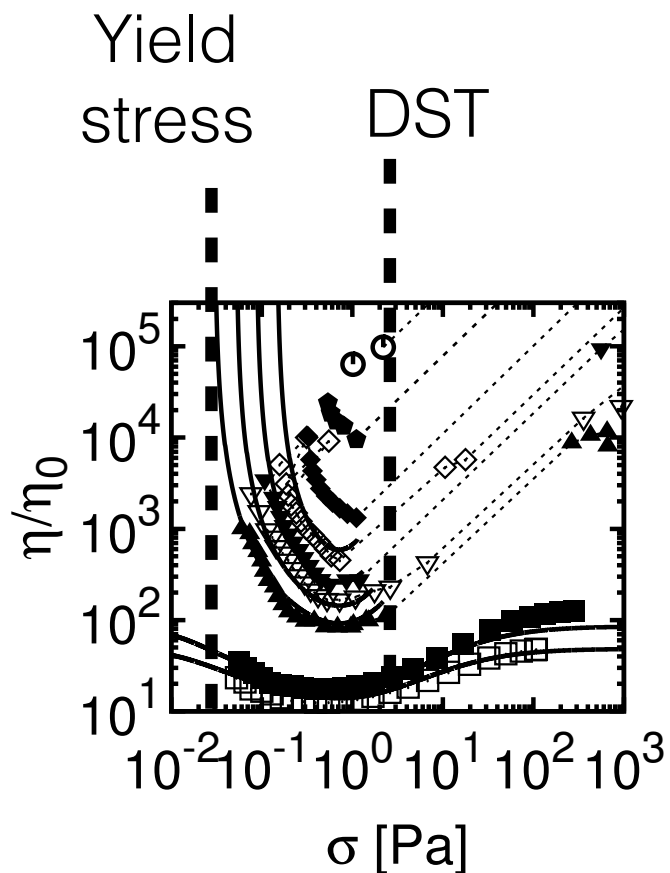
$$\sigma_A/\sigma^*$$

$$\kappa/\beta$$

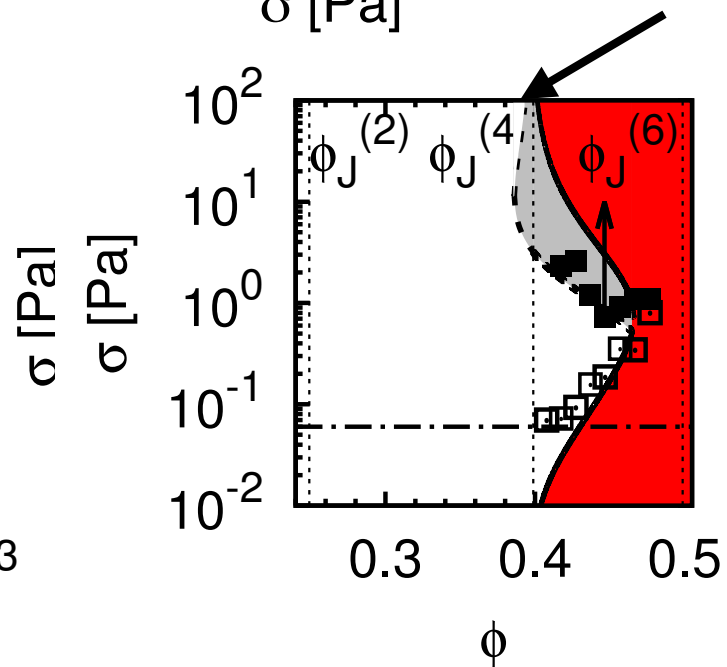
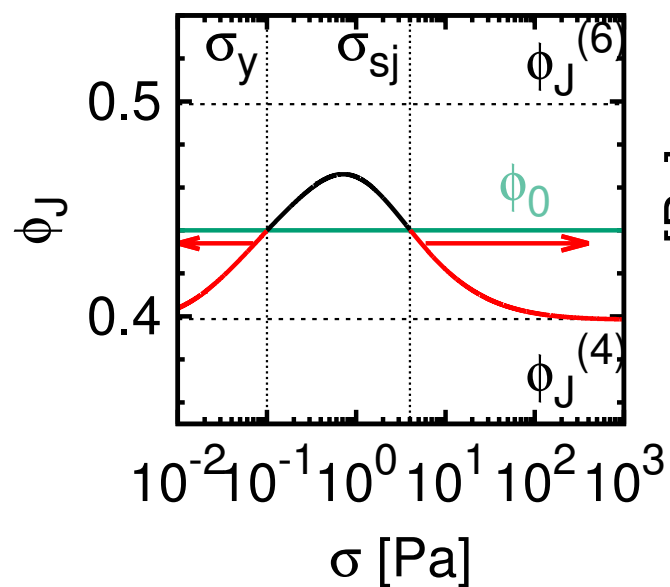
Song et. al.,  
*Nature* (2008)

Case 1:  $\sigma_A/\sigma^* \ll 1$  (Cornstarch in glycerol/water)





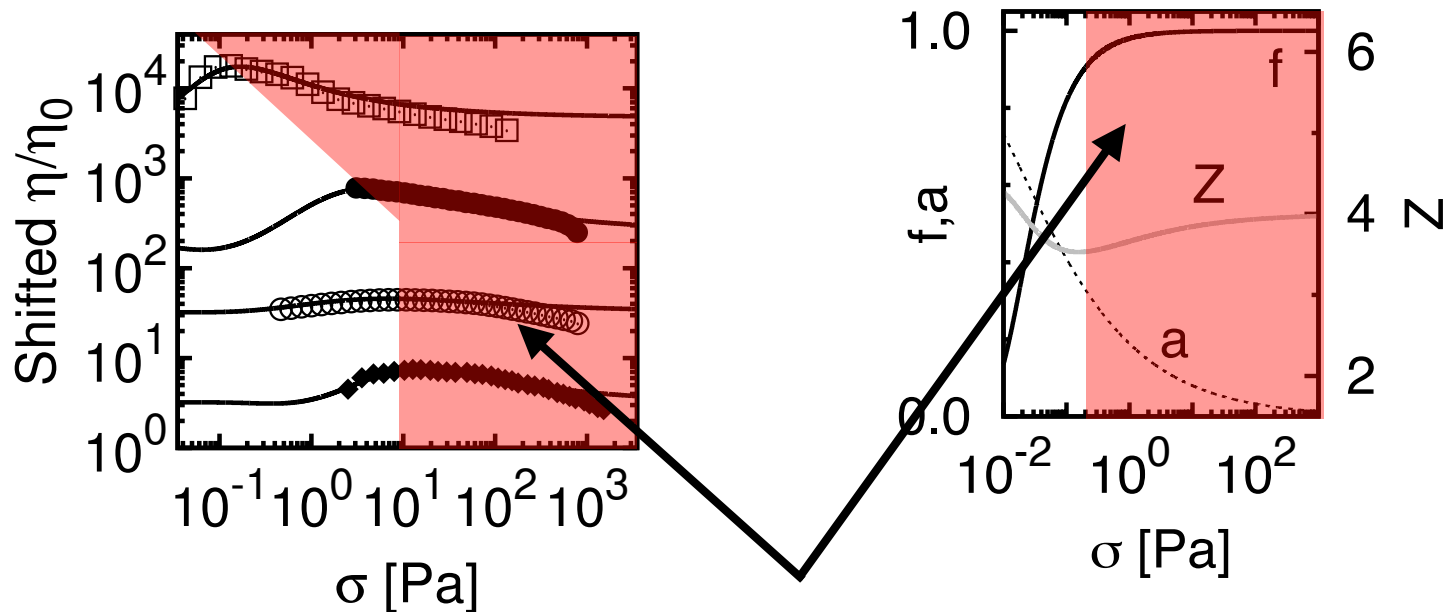
**Yield stress and shear jamming emerge simultaneously**



- Yield stress
- DST stress

Case 2:  $\sigma_A \approx \sigma^*$  (various systems)

Predicts *peaked* flow curves!

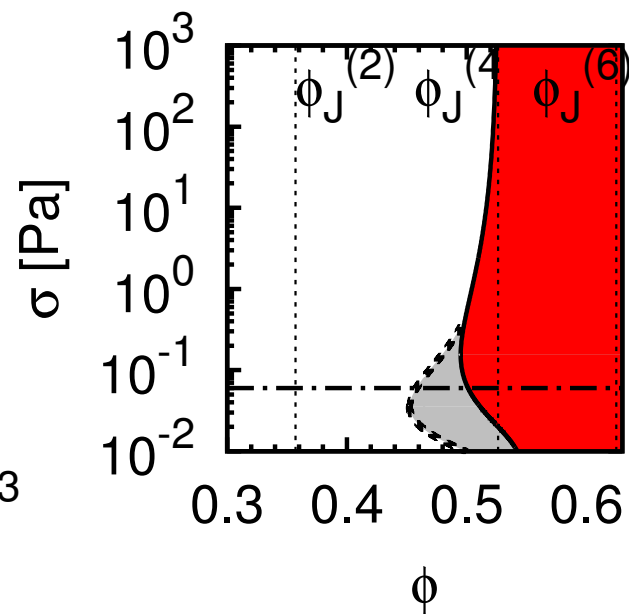
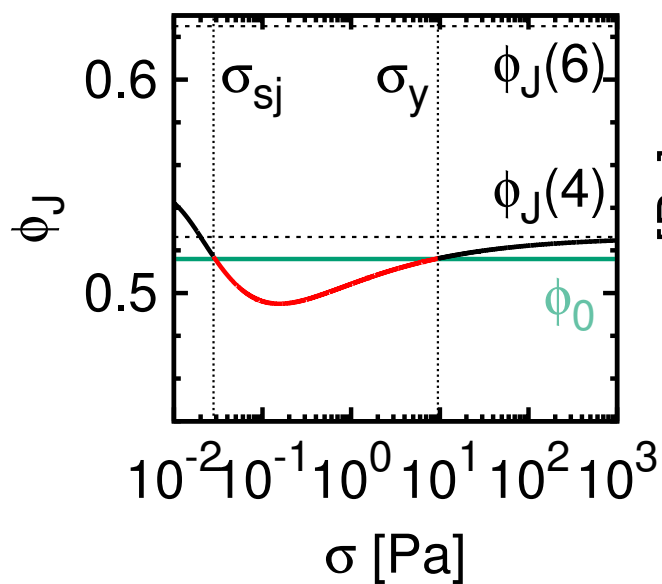
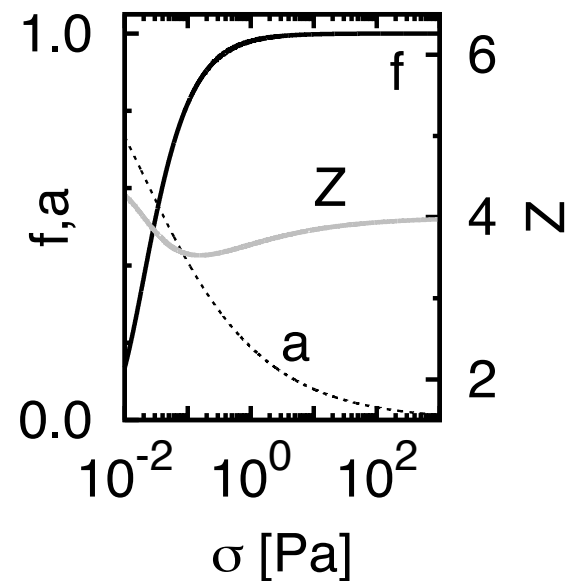
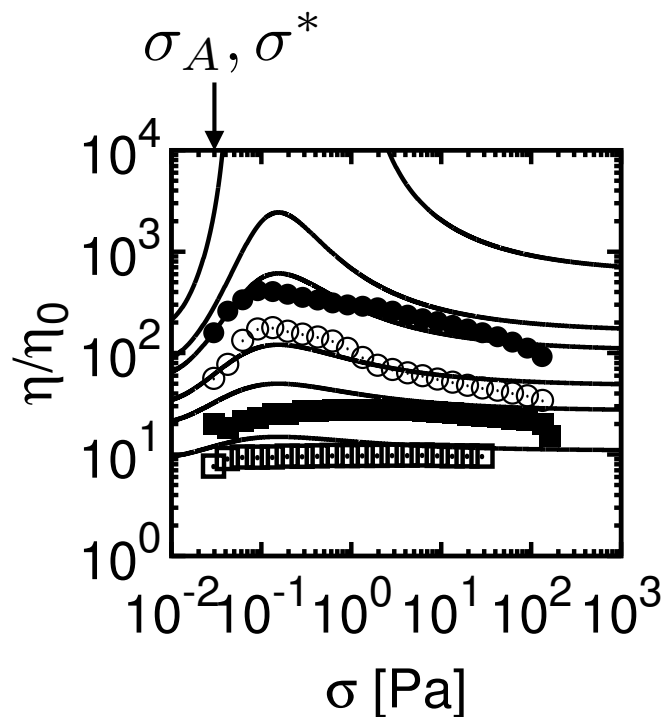


**Gradual breakage of  
adhesive constraints**

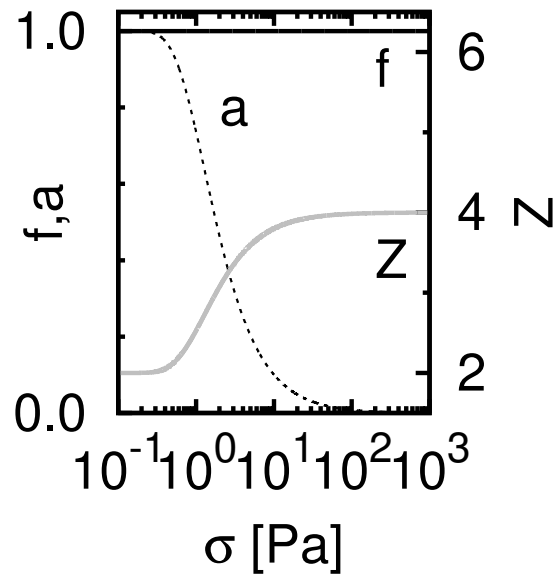
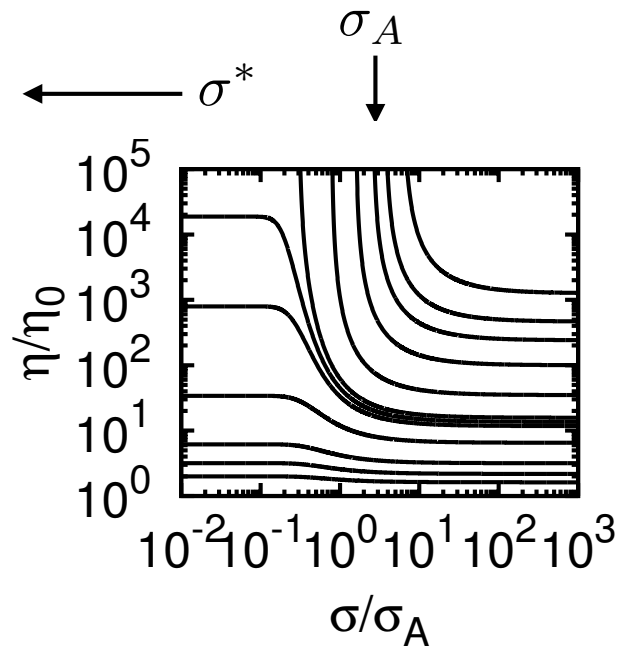
Exact form sensitive to  $\sigma_A/\sigma^*$  and  $\kappa/\beta$   
(and shear history)

Case 2:  $\sigma_A \approx \sigma^*$  (sterically-stabilised 45  $\mu\text{m}$  PMMA in hydrocarbons)

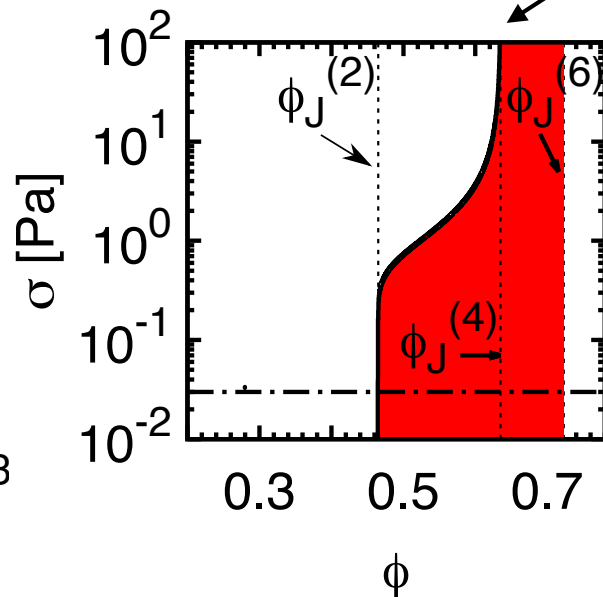
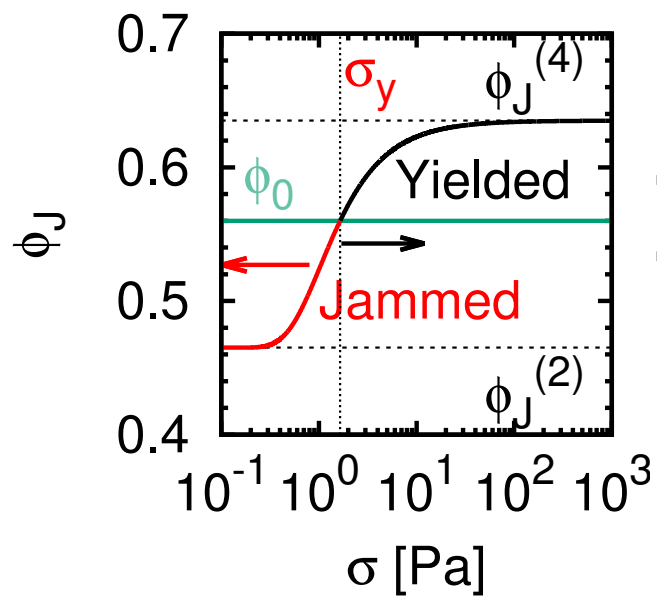
$$\kappa \ll \beta = 1$$



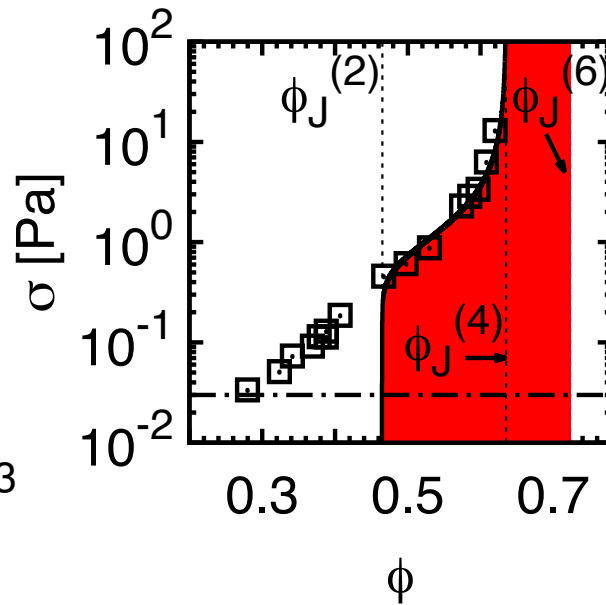
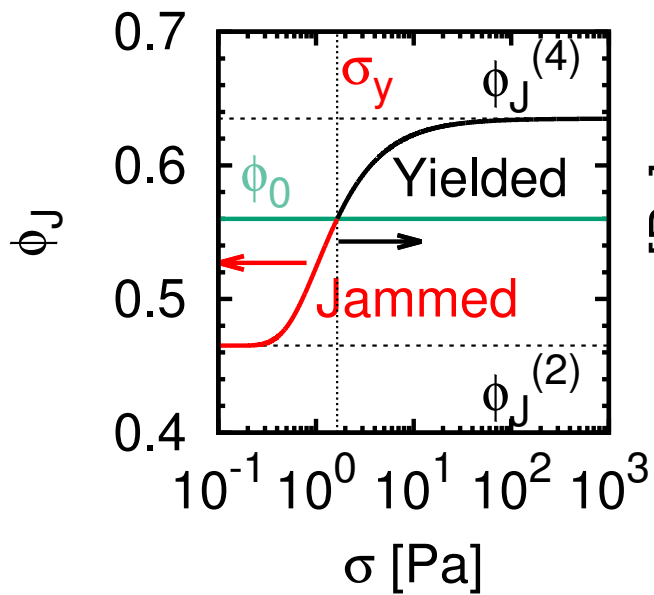
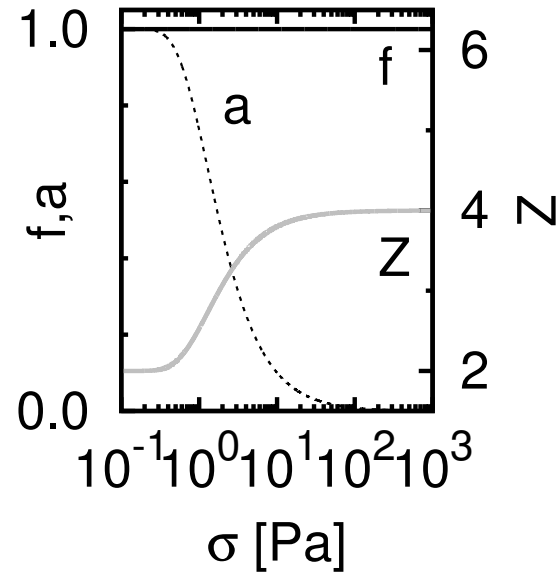
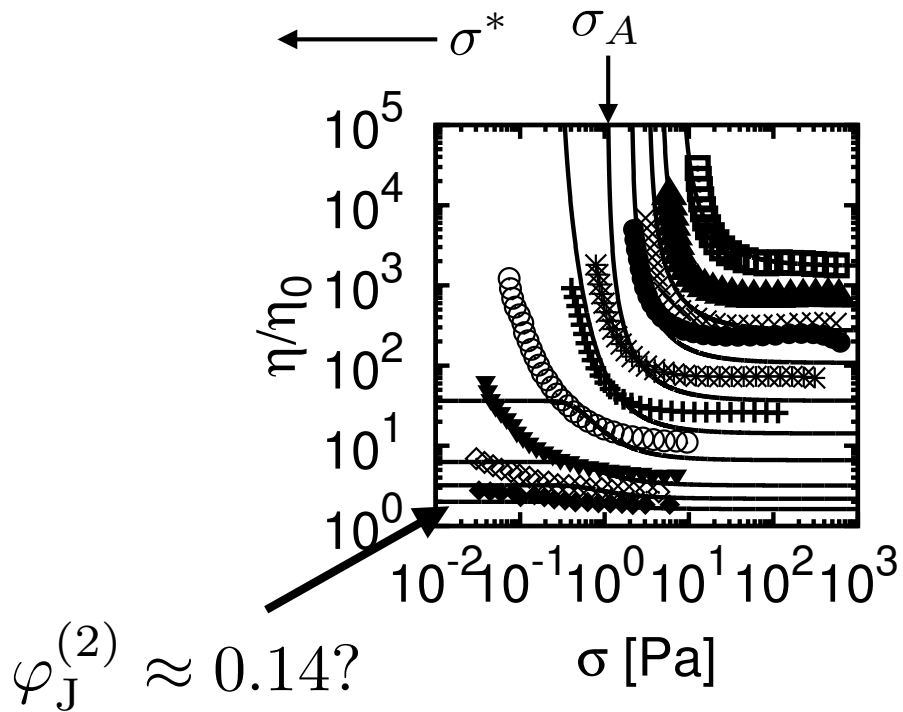
Case 3:  $\sigma_A/\sigma^* \gg 1$



**Yield stress diverges at  $\phi_J^{(4)}$**



Case 3:  $\sigma_A/\sigma^* \gg 1$  (Cornstarch in sunflower oil + lecithin)



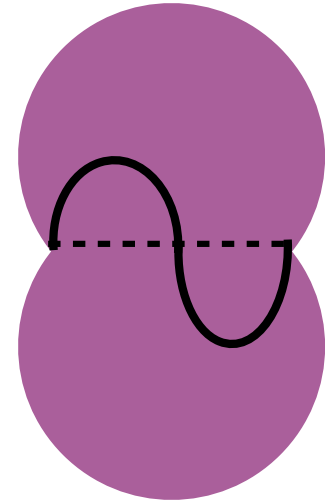
Derived for  $4 \leq Z \leq 6$

$$\phi_J = \frac{Z}{Z + C}$$

Dubious validity for  $Z < 4$ !

# Open questions

- $\sigma_A$  = stress to break adhesive bonds  
e.g., JKR+“pinning”  $\rightarrow$  Bonds break by “peeling”  
*Dominik and Tielens, Phil. Mag. A (1995)*



- $\mathcal{Z}$  provides a “common language” for tribologists and rheologists — how we think about details.
- Hydrodynamics and timescales: implications for  $\mathcal{Z}$   
 $\dot{\gamma} > 0 \implies$  hydrodynamic forces and torques

Standard Reynolds lubrication  $\rightarrow \mathcal{Z} = 6$



Thank you for your attention!

## Edinburgh team

- J. A. Richards (**poster**)
- D. Hodgson
- E. Blanco
- W. C. K. Poon

## Funding



**EPSRC**